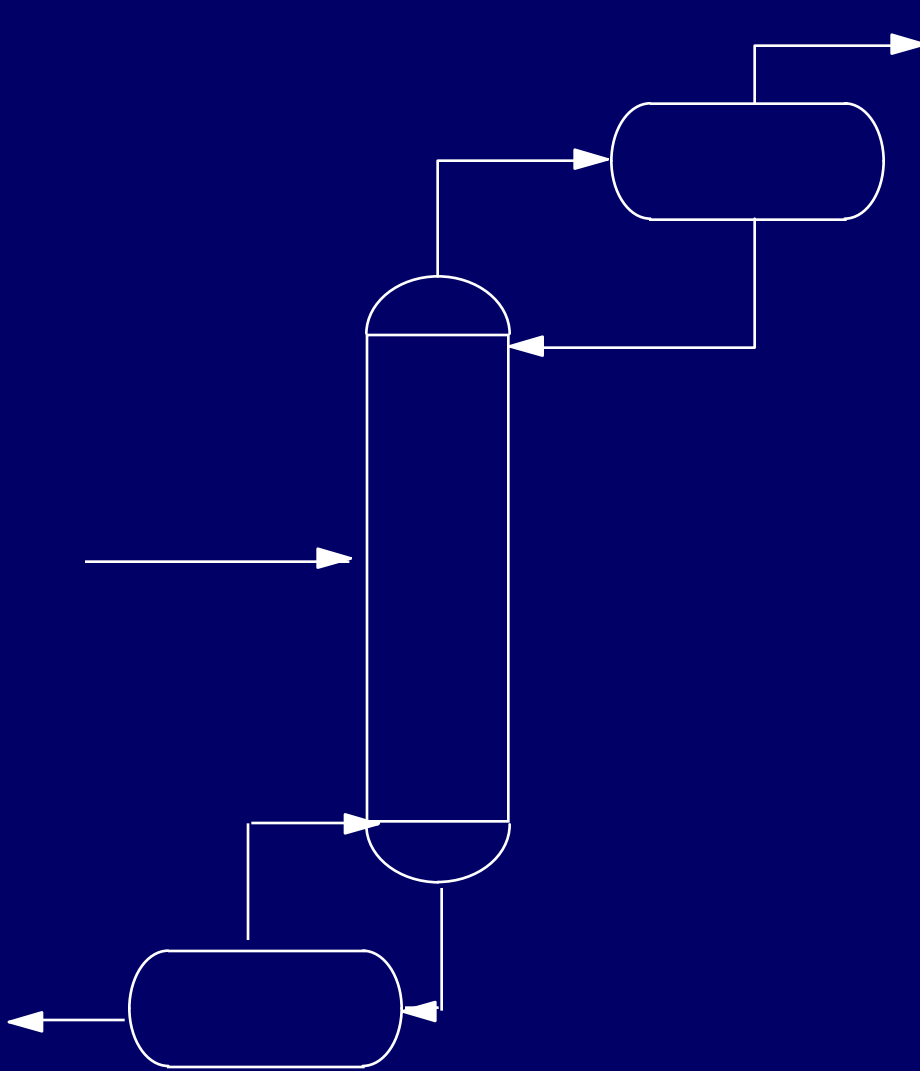


***MultiBatch DS: Professional MultiBatch
Distillation Systems for multiple column
configurations, multiple operating modes,
multiple fractions, and multiple products -- with
multiple levels of models***

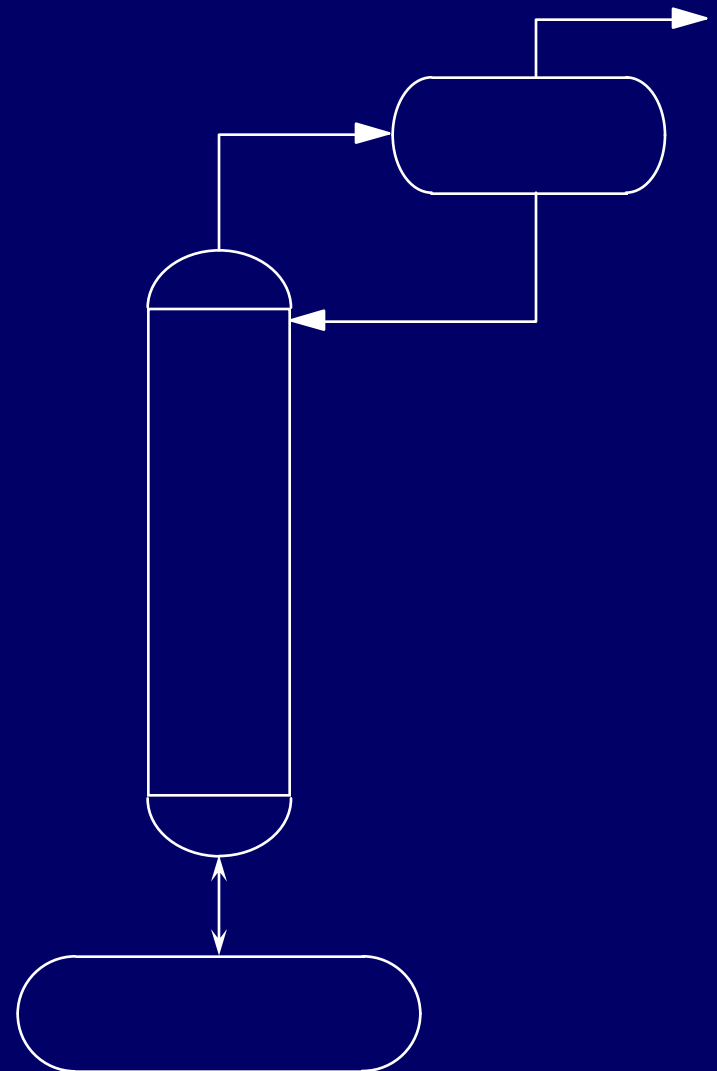
Urmila Diwekar
Stochastic Research Technologies LLC
Crystal Lake, IL
Email: urmila@vri-custom.org

Why Batch Distillation?

Unsteady State Nature of Batch Distillation

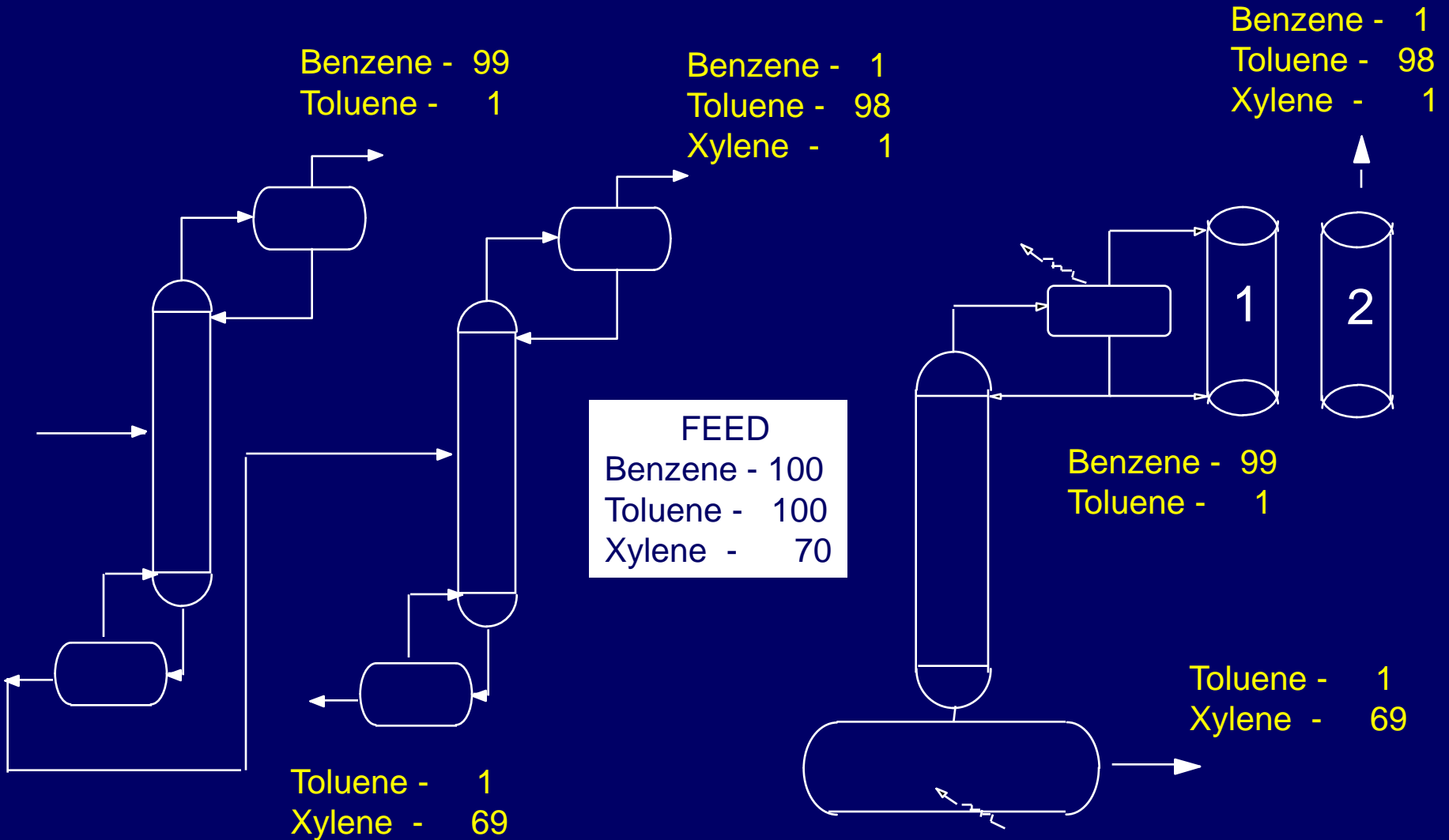


Continuous Distillation

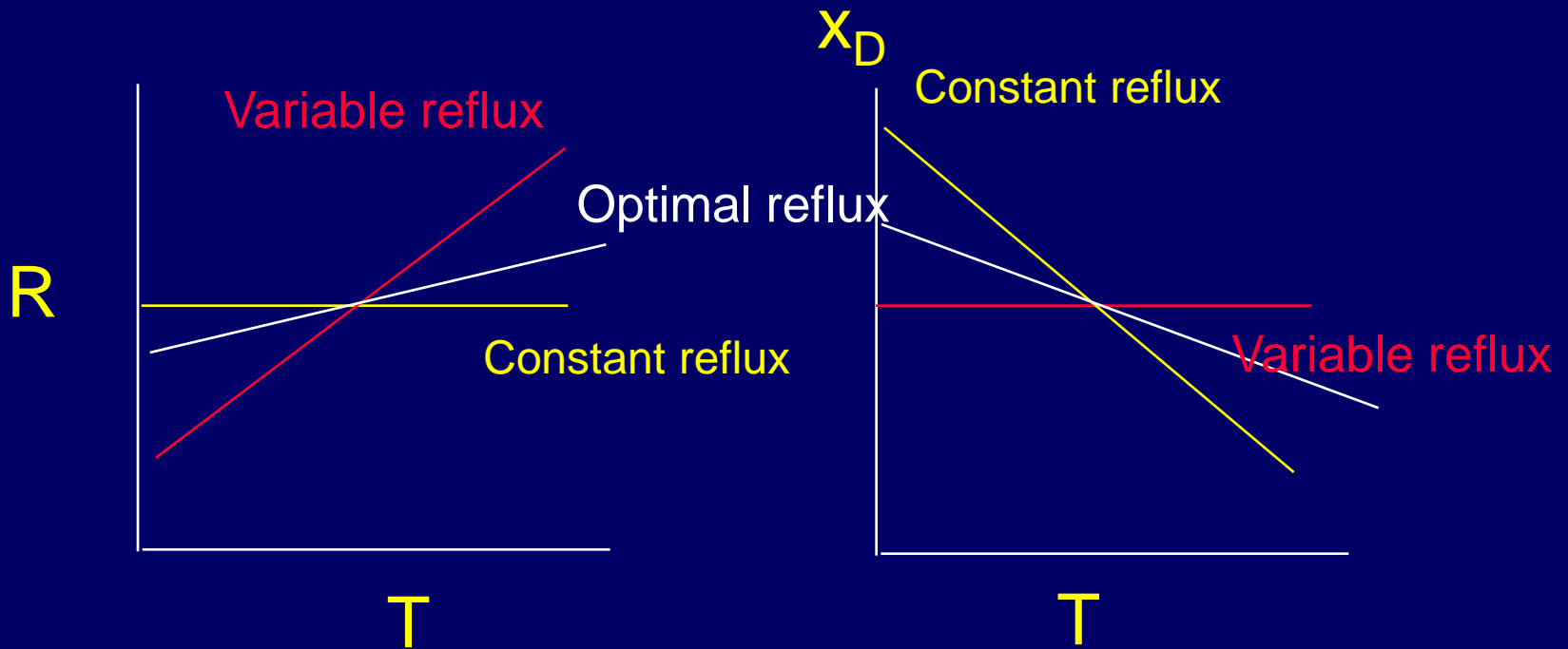


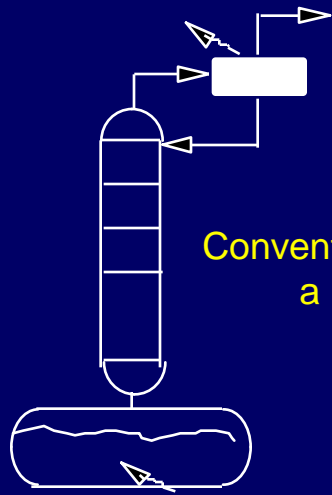
Batch Distillation

Flexibility



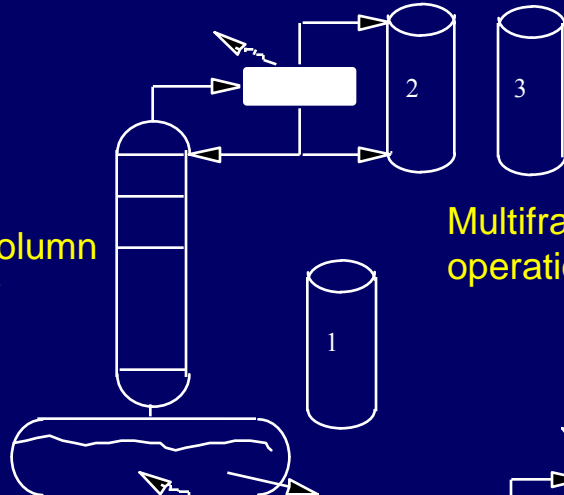
Operating Modes (linear representation)





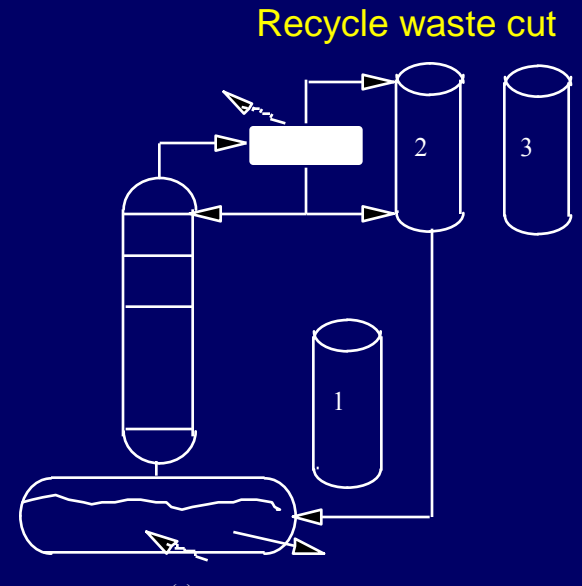
Conventional column
a rectifier

(a)



Multifraction
operation

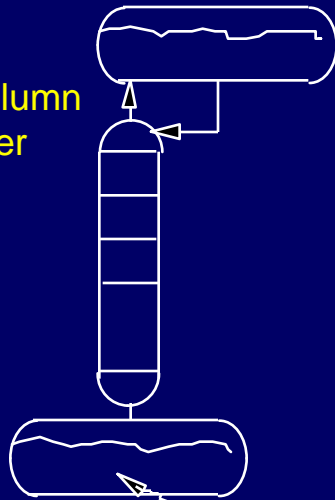
(b)



Recycle waste cut

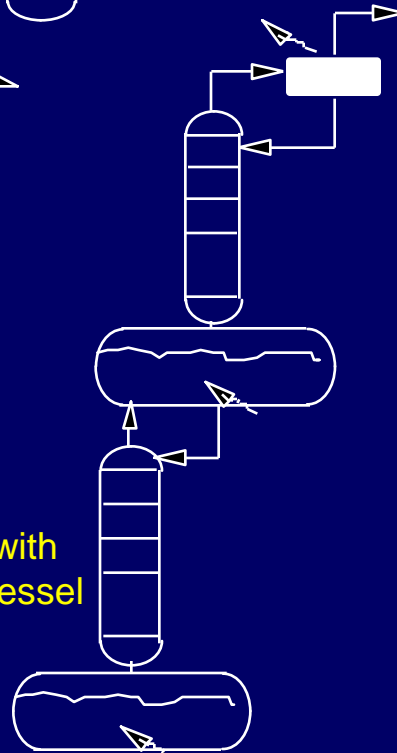
(c)

Inverted column
a stripper



(d)

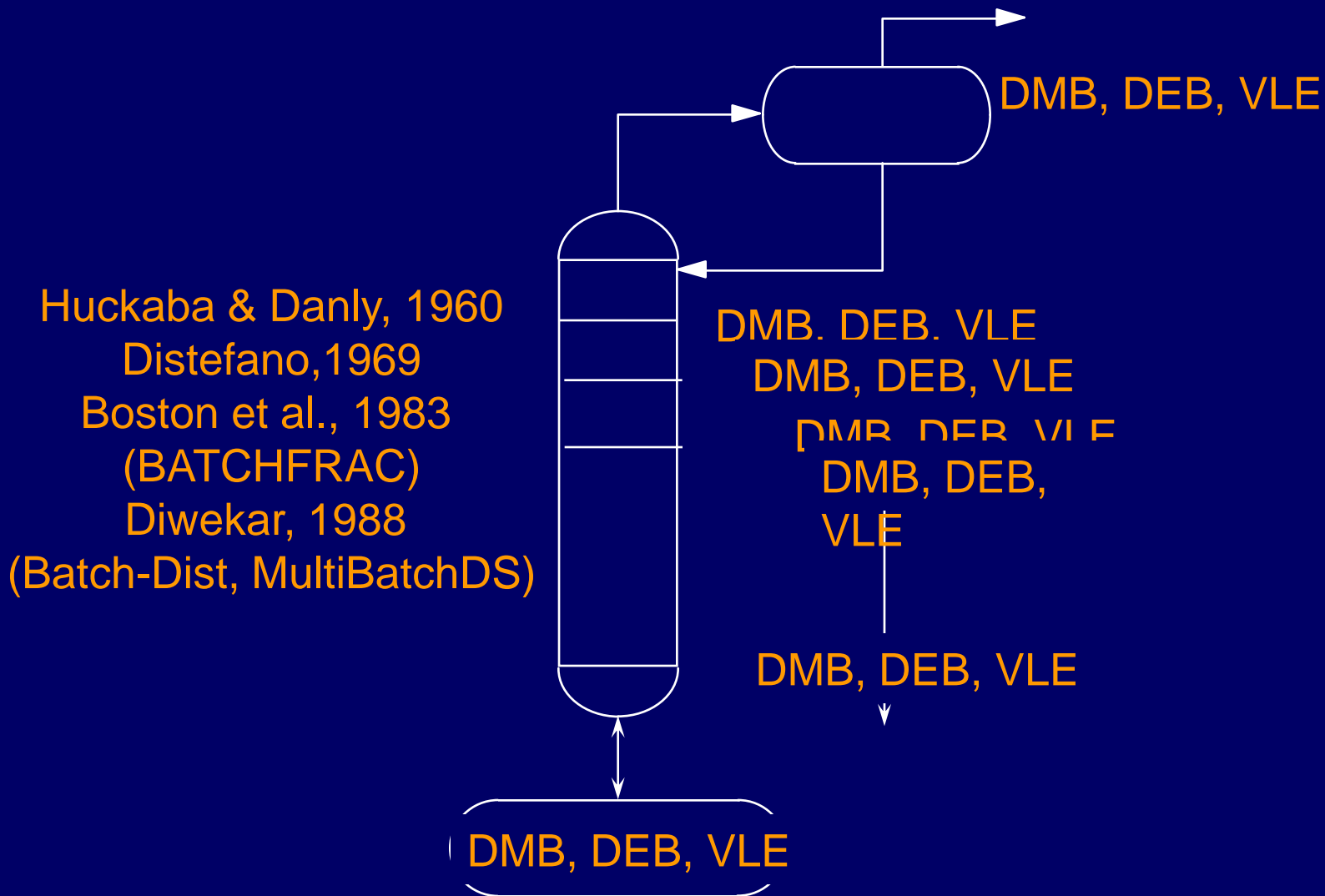
Column with
a middle vessel



(e)

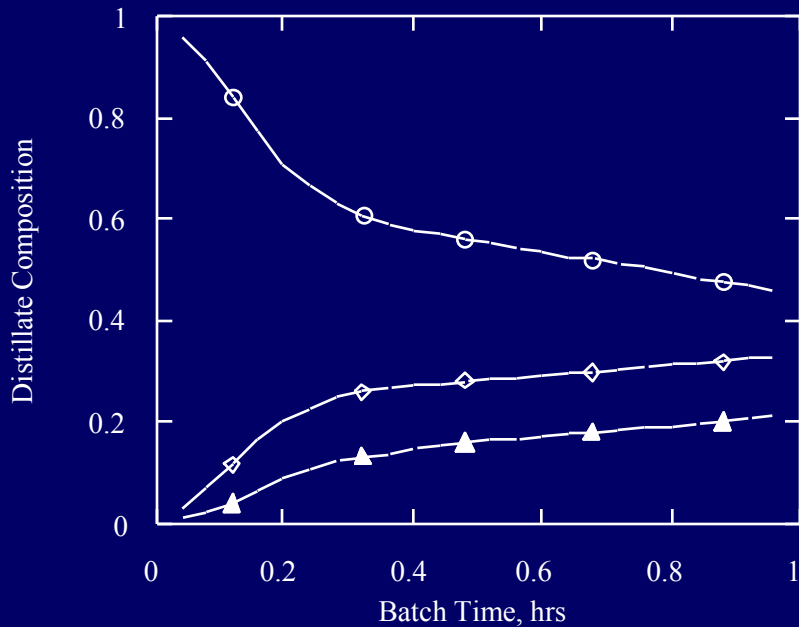
Different column
configurations
including emerging
designs

Rigorous Models



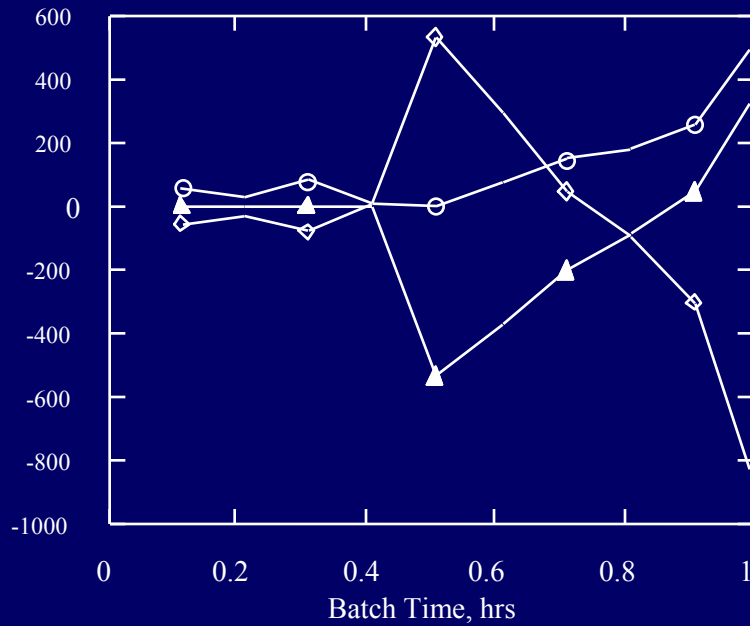
Numerical Integration (contd.)

Stiff Integrator



(a)

Non-Stiff Integrator

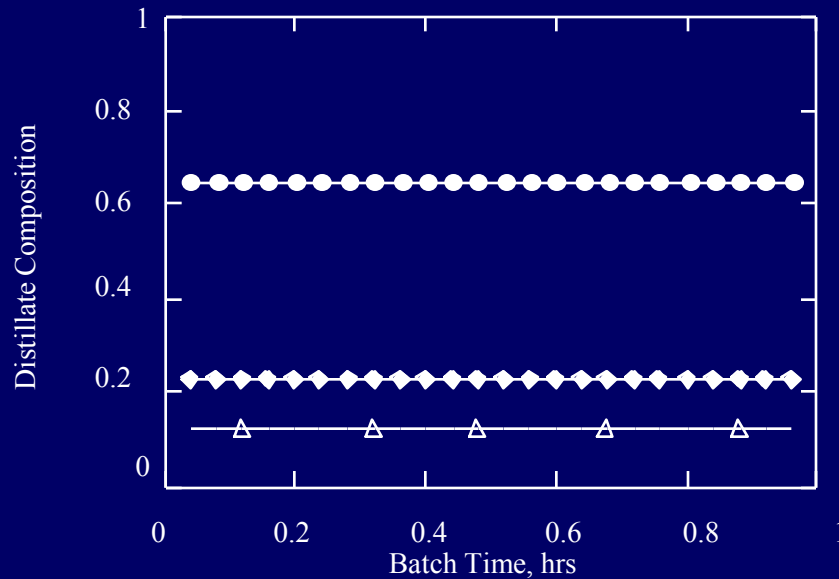


(b)

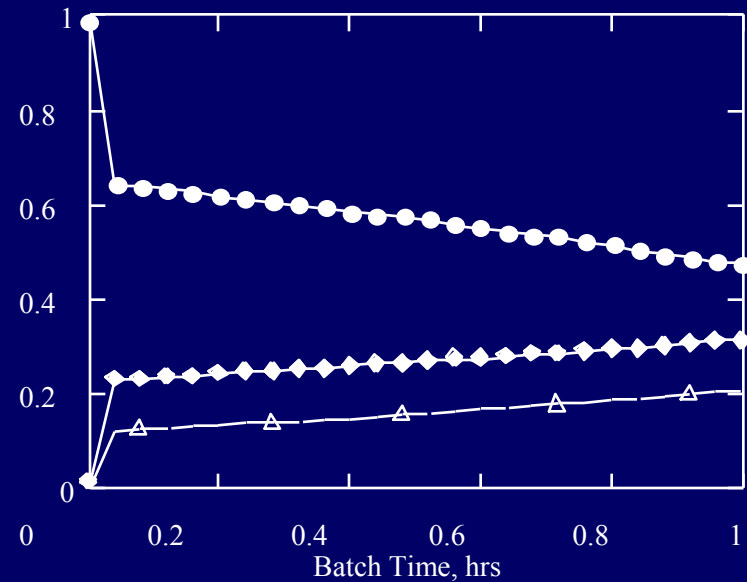
10 % Holdup on plates

Numerical Integration (contd.)

Stiff Integrator



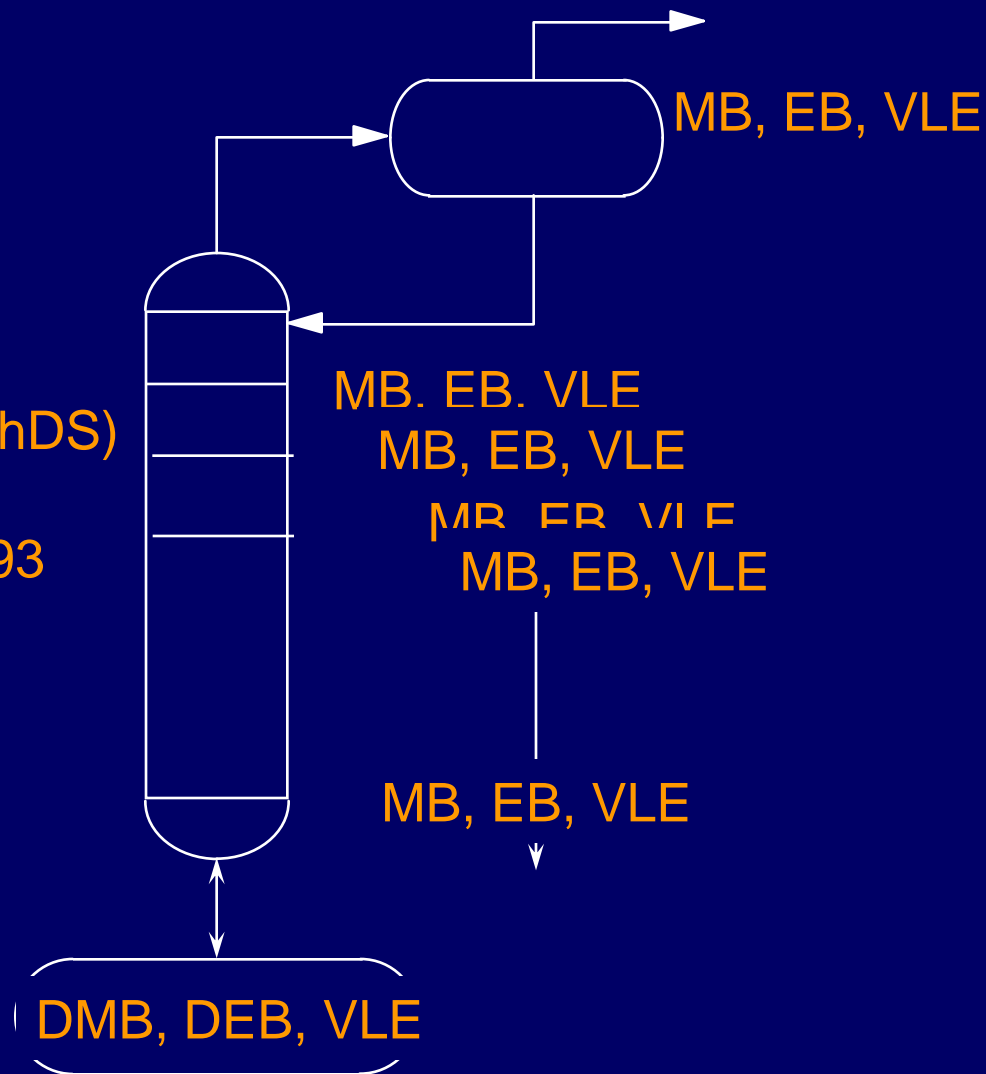
Model Change



1 % Holdup on plates

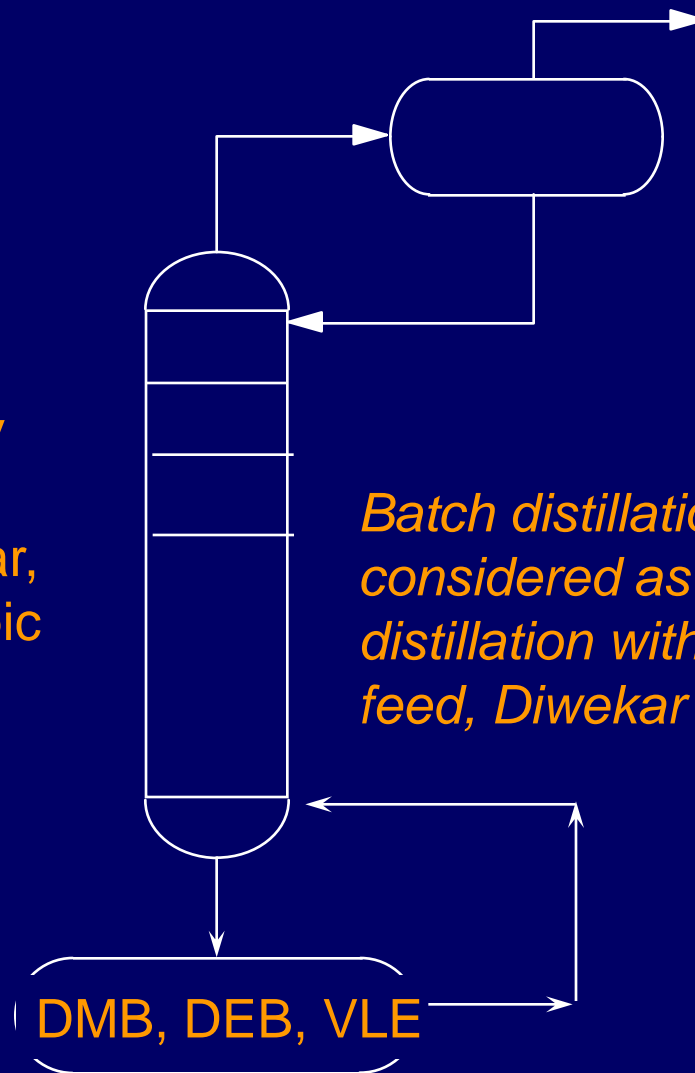
Semi-rigorous Models

Diwekar, 1988
(Batch-Dist, MultiBatchDS)
Doherty &
co-workers, 1990-93



Shortcut Model

Diwekar, 1988
Diwekar, 1991 Binary
Azeotropic Systems
Kalagnanam & Diwekar,
1993, Ternary Azeotropic
Systems



*Batch distillation can be
considered as continuous
distillation with changing
feed, Diwekar 1988*

Batch Distillation Column Software Requirements

Features

Why

Windows

User friendly state of the art input/output interface

Databank

Ability to generate data from structural information

Operations

Constant Reflux
Variable Reflux
Fixed Eqn. Optimal
Optimal Reflux

Yield improvement due to operational flexibility and systematic optimization/optimal control methods

Models

Shortcut
Semirigorous
Reduced Order
Rigorous

Hierarchy of models for numerical stability, design feasibility, and advanced system designs.

Options

Design Feasibility
Optimization
Reactive Distillation
3 phase Distillation
Uncertainty Analysis

Advanced features

Configurations

Semi-batch
Recycle waste cut
Rectifier
Stripper
Middle Vessel

Emerging designs provide promising directions for cost effective designs to obtain purer products

TABLE 10.1

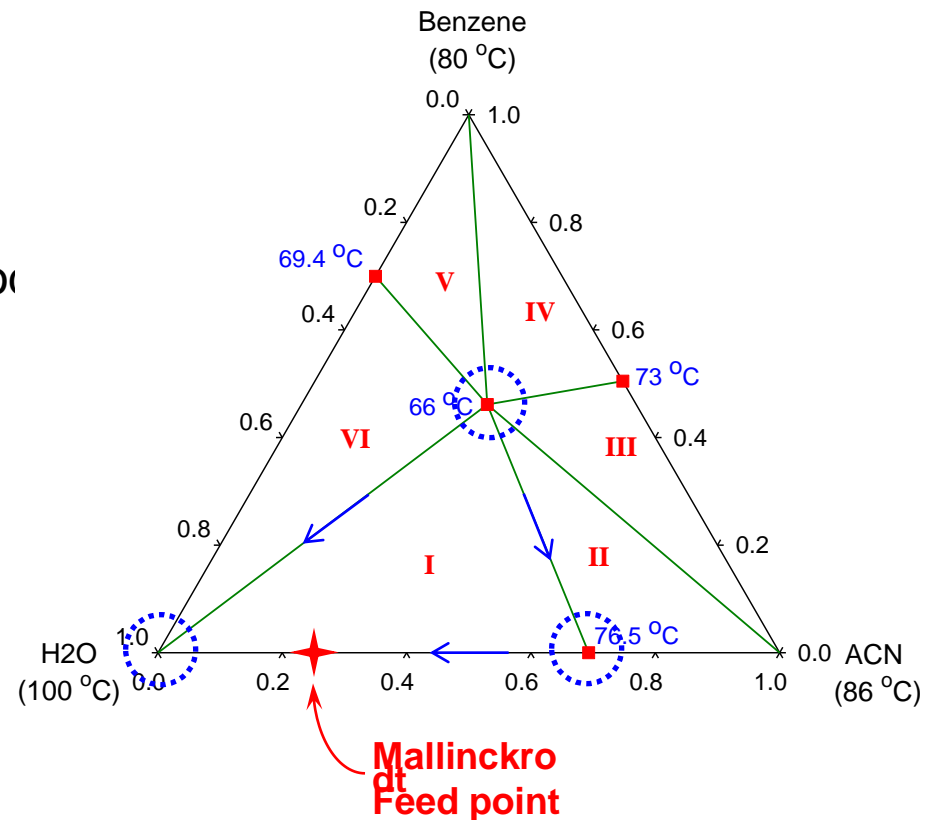
Comparison of Software Packages

Features	CHEMCAD BATCH	BATCHSEP	MultiBatch <i>DS</i>
Databank	CHEMCAD	ASPEN PLUS	CRANIUM
Operations			
Constant Reflux	Yes	Yes	Yes
Variable Reflux	No	Yes	Yes
Optimal Reflux	No	No	Yes
Optimal Reflux Fixed Equation	No	Yes	Yes
Models			
Shortcut	No	No	Yes
Low Holdup Rigorous/Semirigorous	Yes	No	Yes
Reduced Order	No	No	Yes
Rigorous	Yes	Yes	Yes
Configurations			
Rectifier	Yes	Yes	Yes
Semi-batch	No	Yes	Yes
Recycle waste cut	No	Yes	Yes
Stripper	No	No	Yes
Middle Vessel Column	No	No	Yes
Options			
Design Feasibility	No	No	Yes
Optimization	No	Yes	Yes
Reactive Distillation	No	Yes	Yes
3 phase Distillation	Yes	Yes	Yes
Uncertainty Analysis	No	No	Yes

Industrial Case Study 2

Green Solvent Selection & Solvent Recycling

- Acetonitrile(ACN)/Water mixture from peptide drug processes
- Complex thermodynamic system
- Azeotropic agents (Smallwood 1993)
 - ☞ Benzene
 - ☞ Trichloroethylene
 - ☞ Diisopropyl ether
- **Integrated approach**
 - ☞ Batch column configuration
 - ☞ using MultiBatchDS
 - ☞ EBS selection - Discrete optimization

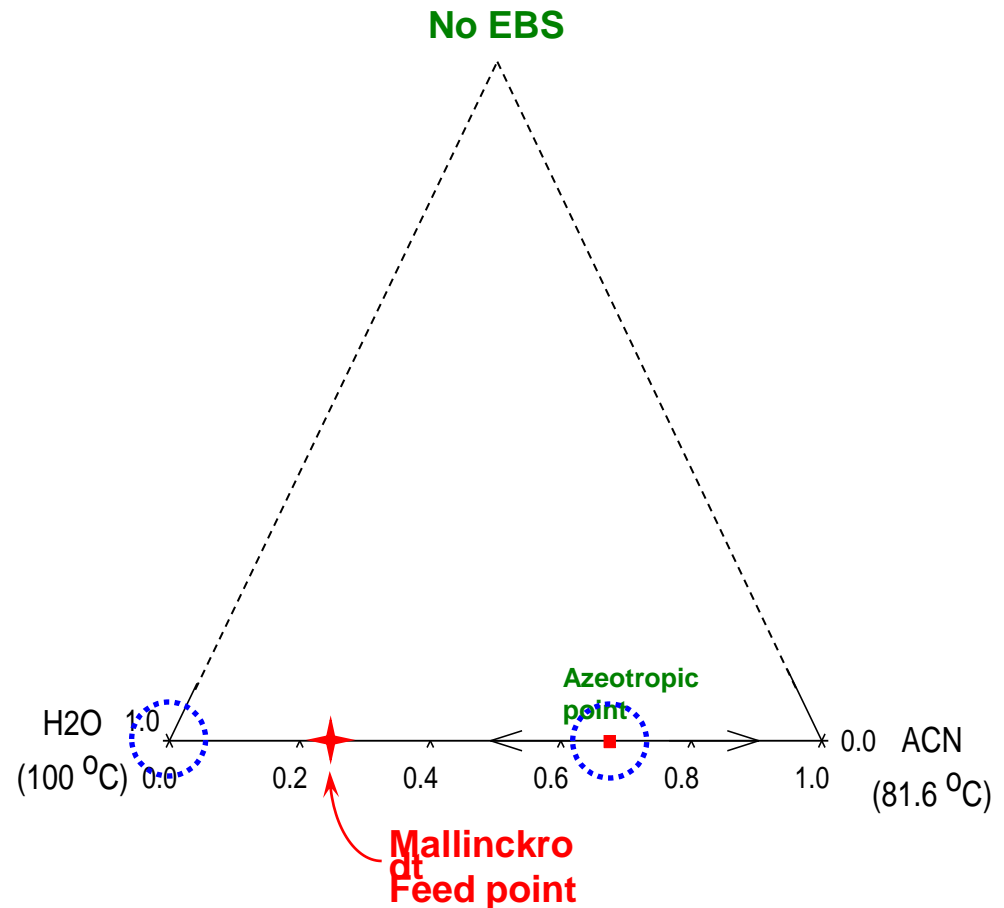


Two Campaigns

□ Campaign I

- 📄 Pure water removal
- 📄 Optimal configuration ⇒ middle vessel column
- 📄 H₂O recovery = 86% (Waste reduced)

- 📄 H₂O recovery in a *rectifier* at *Mallinckrodt* experiments = 61%



Two Campaigns... cont'd

□ Campaign II

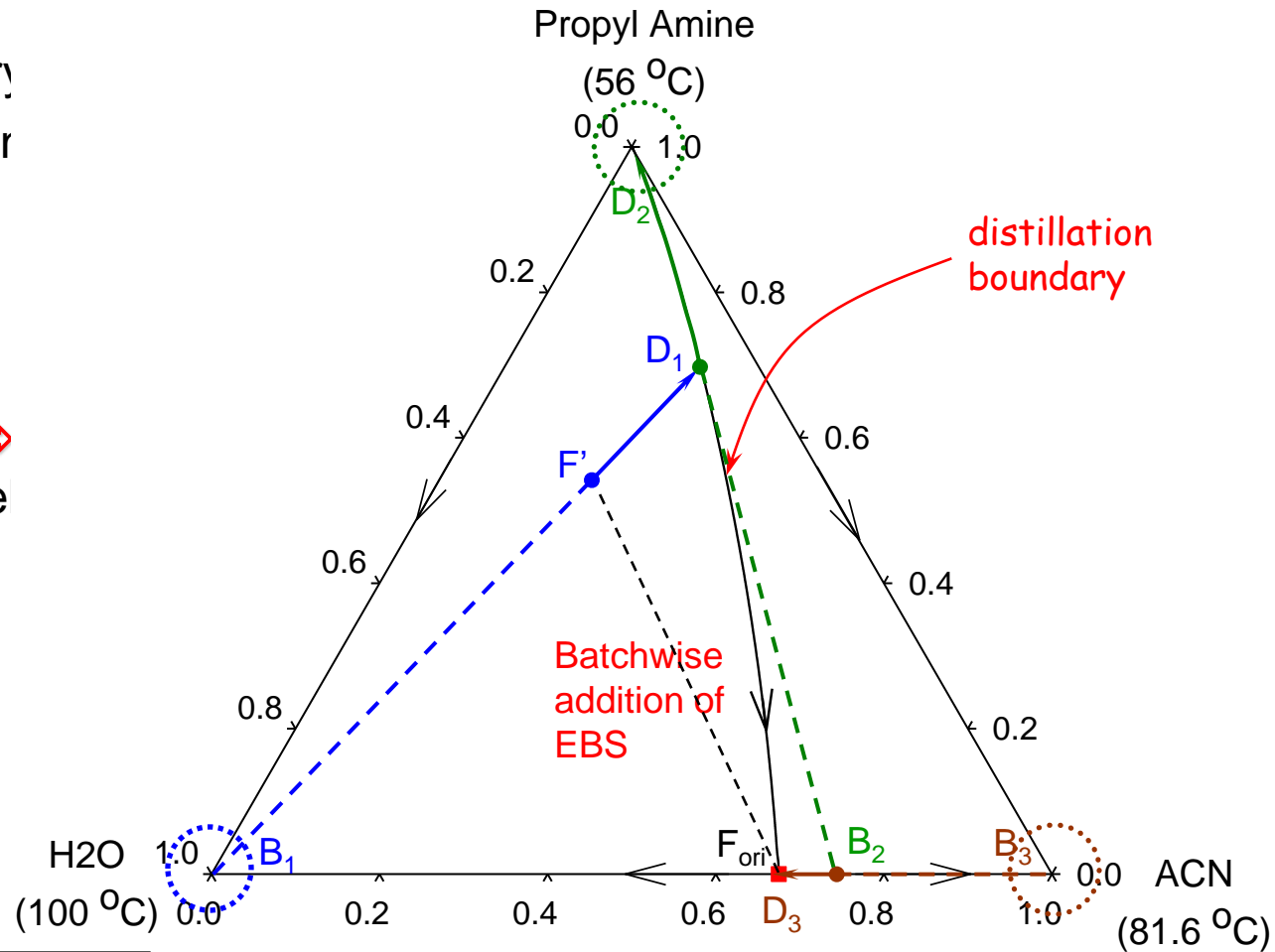
ACN recovery

EBS selector

Propyl amine

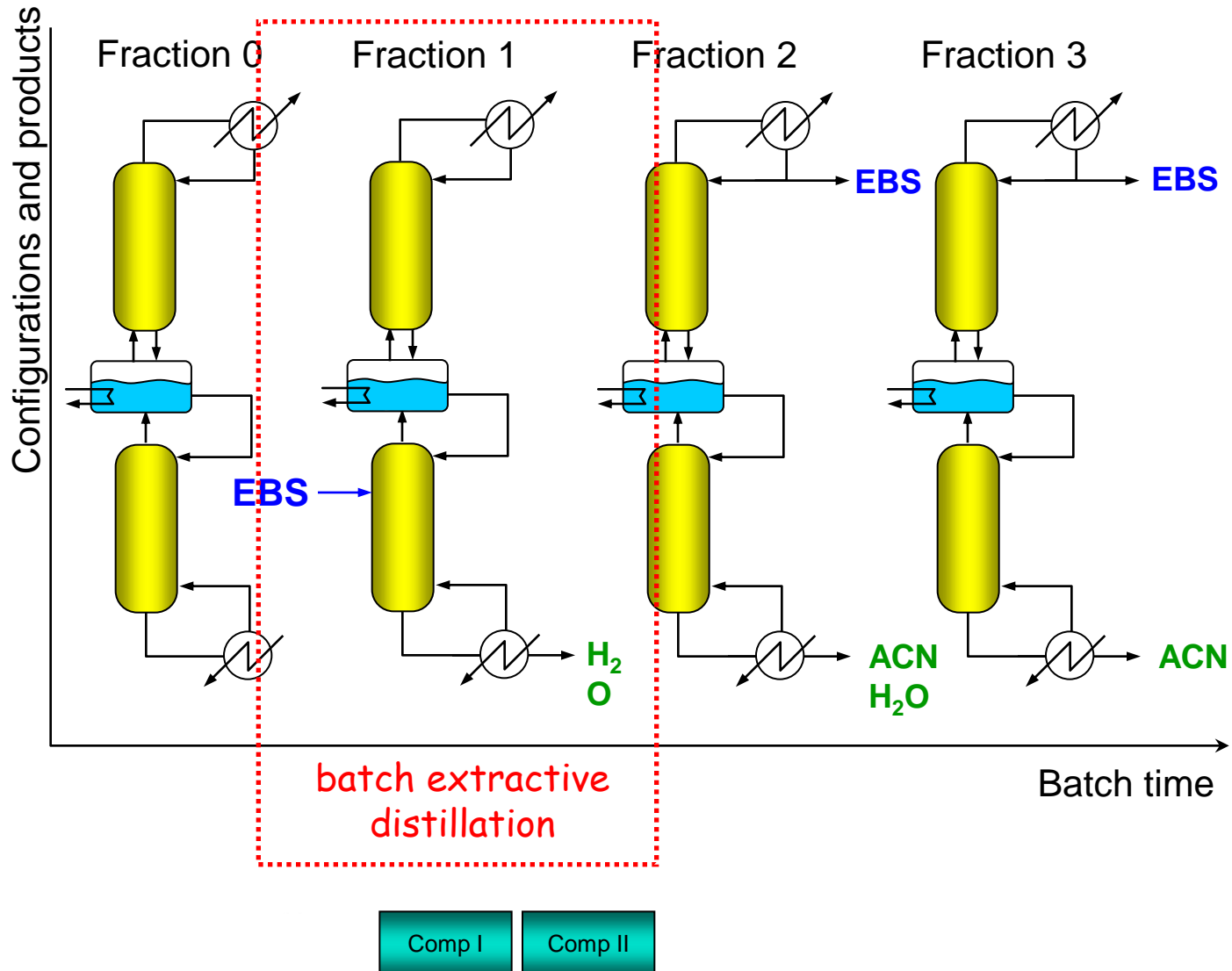
Acetone

Product sequences → middle vesse column



CAMD

Operations for Campaign II



Results and Conclusions of Case Study

- The *first* analysis for the integration of EBS selection and IPS recycling in **batch** processes
- Optimal configuration: Middle vessel column
- EBS selection for batch **extractive** distillation ⇒ Pareto solution
 - 📄 Propyl amine (Recovery: H₂O=98% and ACN=49%)
 - 📄 Acetone (Recovery: ACN=68% and H₂O=43%)

Summary

- Batch Distillation Column Design
 - Unsteady state nature
 - Number of models
 - Flexibility
 - Different modes of operation
 - Different column configurations
- *MultiBatchDS* offers **multiple column configurations, multiple operating modes, multiple fractions, and multiple products -- with multiple levels of models**